

AMENDMENTS TO THE SPECIFICATION:

Please replace the paragraph beginning on page 3, line 14, as follows:

However, these soft resins have poor compatibility with polylactic acid, and there are several problems upon practical use for producing a film, a filament and the like when it is simply melted and mixed. For example, upon molding a film and a filament, because they ~~are~~ do not sufficiently attain uniform mixing even when they are subjected to heat melting and kneading in an extruder, ~~to cause~~ viscosity unevenness, unevenness in thickness of a film and unevenness in diameter of a thread occur, and furthermore, breakage of a film and breakage of a thread occur, whereby stable molding is difficult ~~to be carried out~~.

Please replace the paragraph beginning on page 7, line 3, as follows:

[4] A lactic acid-based resin composition described ~~anyone~~ in any one of items [1] to [3], wherein the mixture (A) of the polylactic acid (a1) and the aliphatic polyester (a2) has a mixing ratio of from 80 to 20 parts by weight of the aliphatic polyester (a2) per from 20 to 80 parts by weight of the polylactic acid (a1).

Please replace the paragraph beginning on page 7, line 9, as follows:

[5] A lactic acid-based resin composition described ~~anyone~~ in any one of items [1] to [4], wherein the aliphatic polyester (a2) is polybutylene succinate and/or polycaprolactone.

Please replace the paragraph beginning on page 7, line 12, as follows:

[6] A molded article comprising a lactic acid-based resin composition described in ~~anyone~~ any one of items [1] to [5].

Please replace the paragraph beginning on page 14, line 5, as follows:

1) a method as shown in Production Example 51, in which caprolactone is ~~onee~~ first subjected to ring opening polymerization in the presence of a catalyst and an aliphatic alcohol to obtain the polymer, and then polymerization is carried out with lactide charged (two-step ring opening polymerization), and

Please replace the paragraph beginning on page 14, line 11, as follows:

2) a method as shown in Production Example 510, in which polylactic acid, which is ~~onee~~ first directly obtained by dehydration polycondensation, and the other aliphatic polyester are mixed and subjected to dehydration polycondensation in the presence of a catalyst and an organic solvent (two-step dehydration polycondensation) can be exemplified.

Please replace the heading on page 23, line 3, as follows:

EXAMPLE EXAMPLES

Please replace the paragraph beginning on page 23, line 12, as follows:

It was measured by ~~gal~~ gel permeation chromatography (GPC) by the polystyrene standard at a column temperature of 40°C with chloroform as a solvent.

Please replace the paragraph beginning on page 26, line 2, as follows:

293.0 kg of diphenyl ether and 2.02 kg of metallic tin were added to 50.5 kg of 1,4-butanediol and 66.5 kg of succinic acid, and heated and agitated at 130°C and 140 mmHg for 7 hours with distilling off water to form an oligomer. A ~~DienStark~~ Dean-Stark trap was attached thereto, and azeotropic dehydration was carried out at 140°C and 30 mmHg for 8 hours. Thereafter, a tube filled with 40 kg of molecular sieve 3A was attached so that the distilled solvent was passed through the molecular sieve tube and was returned to the reactor, followed by agitating at 130°C and 17 mmHg for 49 hours. The reaction mass was dissolved in 600 L of chloroform and was added to 4 kL of acetone to effect reprecipitation, and then sludging was carried out with an isopropyl alcohol (hereinafter abbreviated as IPA) solution of HCl (HCl concentration: 0.7 wt%) for 0.5 hour, followed by filtering. After washing the resulting cake with IPA, it was dried under reduced pressure at 60°C for 6 hours, so as to obtain polybutylene succinate (hereinafter abbreviated as PSB). The polymer had a molecular weight of 140,000 and exhibited an yield of 92%.

Please replace the paragraph bridging pages 30 and 31, as follows:

100 g of 90% L-lactic acid and 450 mg of tin powder were charged in a reactor having a ~~Dien-Stark~~ Dean-Stark trap, and water was distilled off at 150°C and 35 mmHg for 3 hours under agitation, followed by further agitating for 2 hours at 150°C and 30 mmHg, so as to form an oligomer. 210 g of diphenyl ether was added to the oligomer, and an azeotropic dehydration reaction was carried out at 150°C and 35 mmHg. Water and the solvent thus distilled off were separated by a water separator, and only the solvent was returned to the reactor. Polylactic acid in the reaction mass had a weight average molecular weight of 7,500.

Please replace the paragraph beginning on page 37, line 2, as follows:

0.5 part by weight of the block co-polyester obtained in Production Example 5-10 was mixed with 60 parts by weight of the polylactic acid obtained in Production Example 1 and 40 parts by weight of Celgreen PH7 (a trade name, produced by Daicel Chemical Industries, Ltd.) as polycaprolactone, and it was pelletized at 190°C by using a biaxial extruder. The resulting pellets were dried at 80°C for 8 hours. The pellets were subjected to injection molding ~~to in~~ a metallic mold set at from 10 to 30°C by using an injection molding machine having a dehumidifying dryer at a cylinder temperature of from 140 to 220°C and a ~~diee~~ die temperature of from 170 to 190°C, so as to obtain a molded article of a dumbbell piece for tension and flexure. The resulting dumbbell piece had a flexural strength of 65 MPa, a flexural elastic modulus of 2,200 MPa, a tensile strength of 55 MPa and an elongation rate of 220%.

Please replace the paragraph beginning at page 38, line 6, as follows:

The pellets were spun by using a dry spinning machine having a dehumidifying dryer ~~with~~ with a ~~die~~ die having a pore diameter of 0.2 mm and a number of pores of 20 at a temperature of 230°C to obtain a ~~semistretched~~ semi-stretched thread. The molding property upon molding was that spinning could be carried out in good conditions without thread breakage.

Please replace the paragraph beginning at page 38, line 19, as follows:

The same procedures as in Example 3 were carried out except that the block co-polyester was not used to obtain pellets, and spinning was carried out at a ~~die~~ die temperature of 230°C.

Please replace the paragraph bridging pages 39 and 40, as follows:

Pellets were obtained in the same manner as in Example 4 except that the block co-polyester was not used, and were extruded at a ~~die~~ die temperature of 235°C. The film forming property at this time was that film breakage sometimes occurred, and stable molding could not be carried out. The resulting paper laminated product had a thickness of the resin layer of $23 \pm 7 \mu\text{m}$, and the thickness ~~accuracy~~ accuracy was not very good.

Please replace the paragraph beginning on page 40, line 4, as follows:

1.0 part by weight of the block co-polyester obtained in Production Example 51 was mixed with 60 parts by weight of the polylactic acid obtained in Production Example 2 and

40 parts by weight of the polybutylene succinate obtained in Production Example 3, and it was pelletized at 190°C by using a biaxial extruder, followed by drying at 90°C for 8 hours. By using the pellets, they were melted in an injection stretching blow molding machine at a cylinder temperature of from 140 to 250°C to effect injection molding ~~to~~ in a metallic mold set at from 0 to 50°C, so as to obtain a cold parison in a weight of 40 g. After heating and softening the resulting parison at 100°C, it was moved to the interior of a metallic mold having a bottle shape, into which pressurized air at 1 MPa was blown to effect blow stretching at 3.5 times in the vertical direction and 3 times in the horizontal direction, whereby a cylindrical bottle having a bore diameter of 75 mm, a height of 100 mm and an internal volume of 1,000 ml was obtained. The thickness of the wall was 0.2 mm, and the haze was 2.6%.

Please replace the paragraph bridging pages 42 and 43, as follows:

0.5 part by weight of the block co-polyester obtained in Production Example 51 was mixed with 70 parts by weight of the polylactic acid obtained in Production Example 1 and 30 parts by weight of the polybutylene succinate obtained in Production Example 3, and it was pelletized at 190°C by using a biaxial extruder. The resulting pellets were dried at 80°C for 8 hours. By using the resulting pellets, they were formed into a film by using a 90 mm-extruder having a dehumidifying dryer with a ~~die~~ die width of 1,200 mm and a lip gap of 0.8 mm at a temperature of from 150 to 210°C, so as to obtain a film having a thickness of 100 μ m. The film was slit into a width of 6 mm and stretched 5 times by heat plate stretching at a temperature of from 65 to 80°C, followed by thermal fixing on a heat

plate at from 100 to 120°C. The resulting tape had a width of 3.5 mm, a thickness of 30 μm and a strength of 5.10 ± 0.13 g/d.